Direct Simulation of Hydrodynamically Unstable **Premixed Flames**

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¹Thanks to M. Matalon for helpful discussions.

Outline

Theory of the Instability

Discoverors

Markstein's Analysis

Kuramoto-Mickelson-Sivashinsky Equation

Later Analyses

Numerical Experiments

Requirements for Direct Numerical Simulations (DNS)

Experimental Setup

Results

Summary

Hydrodynamic² Instability

Lev Landau



1908 - 1968

Georges Darrieus



1888 - 1979

²Also Landau-Darrieus, Darrieus-Landau, and Thermo-Expansive ₹ → ₹ ↑ ↑ ↑ ↑

Hydrodynamic² Instability

Lev Landau



Physics, 1962

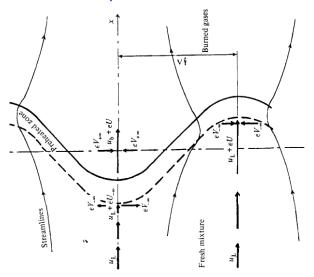
Georges Darrieus



1888 - 1979

²Also Landau-Darrieus, Darrieus-Landau, and Thermo-Expansive (2) Also Landau-Darrieus, Darrieus-Landau, and Thermo-Expansive (3) Also Landau-Darrieus, Darrieus-Landau, and Thermo-Expansive (3) Also Landau-Darrieus (4) A

Non-Mathematical Explanation



"quasi-incompressible fluid + reaction front \Rightarrow instability"

Darrieus' and Landau's Analysis (1930's and 40's)

Imagine a flame in the x-y plane. Assuming

- ► The flame is infinitely thin
- ▶ Fluid satisfies Euler equations on either side of the flame
- ► Flame expands the volume by the factor R
- Local flame speed is s₀
- ▶ Flame location is $y = c \exp(\omega t) \cos(kx)$

then

$$\omega_{LD} = \frac{\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} - \mathcal{R}}{\mathcal{R} + 1} \, s_0 \, k$$

Since $\omega_{LD} > 0$ whenever $\mathbb{R} > 1$, the instability is *unconditional*.

Markstein's Analysis (1951)

Assuming as before, except

▶ Local flame speed is $s = s_0(1 - \mathcal{L}\kappa)$

then

$$\omega_{\text{Ma}} = \frac{\sqrt{\mathcal{R}^3(1-2\mathcal{L}k)+\mathcal{R}^2(1+\mathcal{L}^2k^2)-\mathcal{R}}-\mathcal{R}(1+\mathcal{L}k)}{\mathcal{R}+1}\,s_0\,k\,.$$

In this case $\omega_{\rm Ma}>0$ only when

$$\mathcal{R} > 1$$
 and $\mathcal{L} < 0$ and $k < k_c$, where $k_c = \frac{\mathcal{R} - 1}{2\mathcal{L}\mathcal{R}}$.

Corresponding to the critical wavenumber k_c is the critical wavelength $\lambda_c = 2\pi/k_c$ above which amplification occurs.

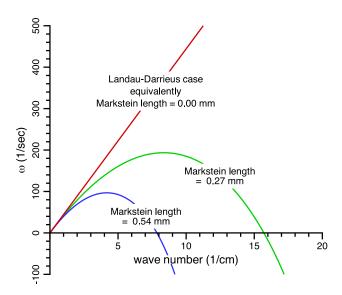
So, more realistically, only perturbations with sufficiently long wavelengths are predicted to be unstable.



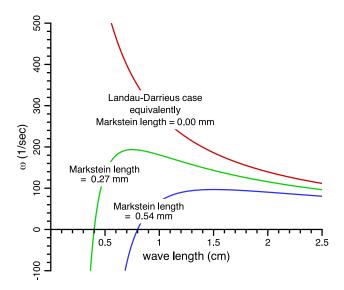
Specific Methane-Air Flame

mechanism	DRM19
ϕ	0.8
$lpha_{0}$	2.24 cm ² /s
${\cal L}$	
Le	0.96
Pr	0.72
${\cal R}$	6.68
s_0	29.27 cm/s
T_0	300 K
T_a	17207 K

Dispersion Relation



Dispersion Relation with Respect to Wavelength



Kuramoto-Mickelson-Sivashinsky Equation (1977)

Thermo-diffusive instability discovered by Zeldovich (1944):

- Analyzed by Zeldovich, Barenblatt, and Sivashinsky
- ▶ Assuming R = 1 ("constant density approximation")
- ▶ Instability requires Le < Le_c < 1</p>

Sivashinsky (1977) combined -diffusive and -expansive effects:

- ▶ Assuming $\mathcal{R} \approx 1$ ("weak thermal limit")
- ▶ Assuming Le ≈ Le_c
- For R = 1 there is a nonparametric evolution equation, the K-M-S equation, with dozens of physical applications
- ► For $\mathbb{R} \neq 1$ and Le = 1 another nonparametric equation describes the purely hydrodynamic instability

$$\frac{\partial u}{\partial \tau} = \frac{\partial^2 u}{\partial \xi^2} - \frac{1}{2} \left(\frac{\partial u}{\partial \xi} \right)^2 + \frac{1}{2\pi} \int_0^\infty \int_{-\infty}^\infty k \, u(x, \tau) \cos k(\xi - x) \, dx \, dk$$



More Realistic Assumptions (1982)

Three papers

- 1. Pelce and Clavin
- 2. Matalon and Matkowsky
- 3. Frankel and Sivashinsky
- Assuming one irreversible reaction
- ► Assuming no restrictions on Le and R
- All found viscosity has no effect
- All have different notation and nondimensionalizations

$$\begin{split} \omega_{\text{FS}} &= \frac{\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} - \mathcal{R}}{\mathcal{R} + 1} s_0 \, k + \left[\frac{\mathcal{R}^2 \log \left(\frac{\mathcal{R}^2 + 2\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + 1}{\mathcal{R}^2 (\mathcal{R} + 1)} \right) - (\mathcal{R} - 1)^2}{2(\mathcal{R} - 1)\sqrt{\mathcal{R}} + 1 - \mathcal{R}^{-1}} \right. \\ &+ \left. \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}} + 1 - \mathcal{R}^{-1} - 1}{2(\mathcal{R} + 1)^2 \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}} + 1 - \mathcal{R}^{-1} - 1}{2(\mathcal{R} + 1)^2 \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}} + 1 - \mathcal{R}^{-1} - 1}{2(\mathcal{R} + 1)^2 \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}} + 1 - \mathcal{R}^{-1} - 1}{2(\mathcal{R} + 1)^2 \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}} + 1 - \mathcal{R}^{-1} - 1}{2(\mathcal{R} + 1)^2 \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right) \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + \mathcal{R} + 2 \right) + \mathcal{R} \left(\mathcal{R} + 2 \right) \right. \\ \left. + \frac{\mathcal{R} \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + 2 \right) + \mathcal{R} \left(\mathcal{R} + 2 \right) \right. \\ \left. + \frac{\mathcal{R} \left(\mathcal{R} + 2 \right) + \mathcal{R} \left(\mathcal{R} + 2 \right) + \mathcal{R} \left(\mathcal{R} + 2 \right) \right. \\ \left. + \frac{\mathcal{R} \left(\mathcal{R} + 2 \right) + \mathcal{R} \left(\mathcal{R} + 2 \right) + \mathcal{R} \left(\mathcal{R} + 2 \right) \right. \\ \left. + \frac{\mathcal{R} \left(\mathcal{R} + 2 \right) + \mathcal{R} \left(\mathcal{R} + 2 \right) + \mathcal{R} \left(\mathcal{R} + 2 \right) \right. \\ \left. + \frac{\mathcal{R} \left(\mathcal{R} + 2 \right) + \mathcal{R} \left(\mathcal{R} + 2 \right) \right. \\ \left. + \frac{\mathcal{R} \left(\mathcal{R}$$

F & S predict unrealistically small $\lambda_c=0.079$ cm.

Matalon, Cui, and Bechtold (2003)

New analysis

- Assuming properties vary through the flame zone
- Viscous terms do not drop out

$$\begin{split} \omega_{\text{MCB}} &= \frac{\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} - \mathcal{R}}{\mathcal{R} + 1} s_0 \, k \\ &- \left[\frac{\mathcal{R} \left(3\mathcal{R}^3 + \mathcal{R}^2 + 4\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}\mathcal{R} + \mathcal{R} - 1 \right)}{4(\mathcal{R} + 1)\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right. \\ &+ \frac{T_a}{T_0} (\text{Le}_{\textit{eff}} - 1) \frac{(\mathcal{R} - 1)^2 \left(\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} + 1 \right) \left(\mathcal{R}^2 + \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}} \right)}{2\mathcal{R}(\mathcal{R} + 1)^2 \sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \\ &+ \text{Pr} \, \frac{(\mathcal{R} - 1)^2 \mathcal{R}}{2\sqrt{\mathcal{R}^3 + \mathcal{R}^2 - \mathcal{R}}} \right] \alpha_0 \, s_0 \, k^2 \end{split}$$

M C & B predict realistic $\lambda_c = 0.48$ cm

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DNS Requirements to Study Natural Flames

1. Spatial resolution requirement:

13 points through the flame zone.

flame zone thickness 0.2 mm \Rightarrow spatial resolution $\Delta x \approx 15\mu$

2. **Temporal duration** requirement:

The flame must traverse, chemically, a significant distance to reveal its natural behavior.

$$\frac{\text{total time}}{\text{flame speed 29 cm/s}} = \frac{60 \times \text{thermal thickness 0.5 mm}}{\text{flame speed 29 cm/s}} = 0.1 \text{ sec}$$

Temporal resolution requirement (CFL stability condition):

$$\Delta t < 0.5 imes rac{\Delta x}{ ext{fastest speed in simulation}}$$

4. Number of time steps required

$$N = \frac{\text{total time}}{\Delta t} > \frac{0.2 \text{ fastest speed}}{\Delta x} = \frac{13,500 \times \text{fastest speed (m/s)}}{\text{speed (m/s)}}$$

Traditional DNS versus low Mach number DNS

```
time steps N=13,500 \times \text{fastest speed in simulation(m/s)}

traditional DNS = ... × sound speed at 2000 K = 10,400,000

low Mach-number = ... × hot gas velocity = 27,500
```

A flame must traverse a significant distance, as a result of chemical reactions, to reveal its natural behavior.

This work uses the low Mach-number combustion software developed at Lawrence Berkeley National Laboratory (LBNL).

- low Mach-number formulation
- adaptive mesh refinement (AMR)
- mixture-averaged transport without cross-diffusion implemented by Day and Bell (2000)



Traditional DNS versus low Mach number DNS

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time steps N=13{,}500 \times \text{fastest speed in simulation(m/s)}
traditional DNS > \dots \times \text{sound speed at } 2000 \text{ K} = 10{,}400{,}000
low Mach-number = \dots \times \text{hot gas velocity} = 27{,}500
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Computational Setup



initial fuel mass consumption

Freely propagating 2D flame

- ▶ CH₄-Air with $\phi = 0.8$
- No gravity
- No radiation losses
- Widths 0.4, 0.8, and 1.2 cm
- ▶ 0.1+ seconds duration
 - Initially randomly wrinkled flame
- Bottom inflow controlled to hold flame stready
- Side boundaries periodic
- Aspect ratio height:width = 5 : 1
- Controlled inflow



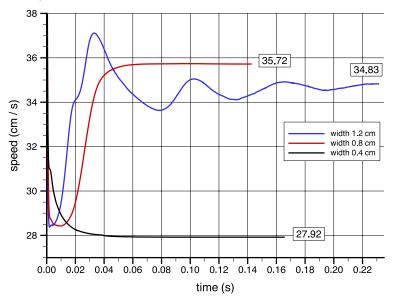
Movies

0.4 cm

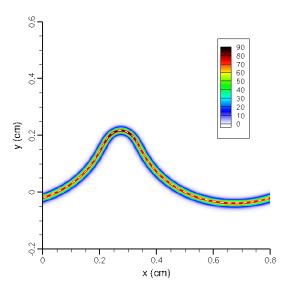
0.8 cm

1.2 cm

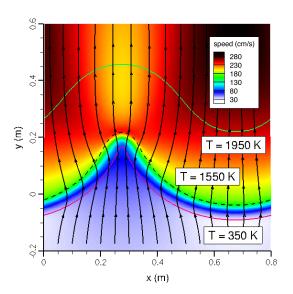
Flame Speed



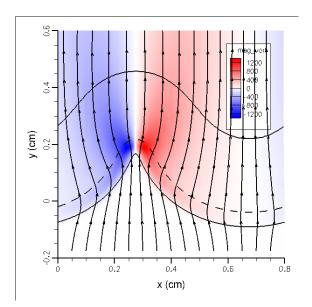
Fuel Consumption Isotherm



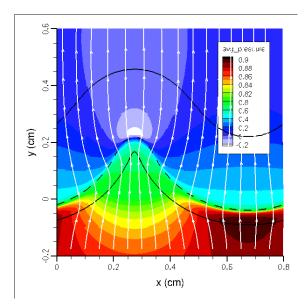
Velocity



Vorticity



Pressure



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- ► Theory has evolved to the point that Matalon et al (2003) appear to give quantitatively correct predictions
- The non-mathematical explanation of Landau appears to most accurately describe the instability
- Contrary to previous simulations, the flame appears not susceptible to "jitters" once it assumes the canonical shape.
- ➤ As the simplest nontrivial flame, it may be used to test many theorized relationships. Suggestions welcome.

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